P TENT COOPERATION TREAT

	From the INTERNATIONAL BUREAU
PCT	To:
NOTIFICATION OF ELECTION (PCT Rule 61.2)	Assistant Commissioner for Patents United States Patent and Trademark Office Box PCT Washington, D.C.20231 ETATS-UNIS D'AMERIQUE
Date of mailing (day/month/year) 11 August 2000 (11.08.00)	in its capacity as elected Office
International application No. PCT/GB99/04156	Applicant's or agent's file reference
International filing date (day/month/year) 09 December 1999 (09.12.99)	Priority date (day/month/year) 09 December 1998 (09.12.98)
Applicant	(0011200)
GANDERTON, David et al	
1. The designated Office is hereby notified of its election maximum. X in the demand filed with the International Prelimina	ary Examining Authority on: (03.07.00)
The International Bureau of WIPO 34, chemin des Colombettes 1211 Geneva 20, Switzerland	Authorized officer Olivia RANAIVOJAONA
Facsimile No.: (41-22) 740.14.35	Telephone No.: (41-22) 338.83.38

P TNT COOPERATION TREAT

To:

From the I	NT	FRNA	TIONA	L BL	JREAU
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PCT

NOTIFICATION OF ELECTION

(PCT Rule 61.2)

Assistant Commissioner for Patents United States Patent and Trademark Office

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GANDERTON, David et al

Applicant

1.	The designated Office is hereby notified of its election made:
	X in the demand filed with the International Preliminary Examining Authority on:
	03 July 2000 (03.07.00)
	in a notice effecting later election filed with the International Bureau on:
2.	The election X was
	was not
	made before the expiration of 19 months from the priority date or, where Rule 32 applies, within the time limit under Rule 32.2(b).

The International Bureau of WIPO 34, chemin des Colombettes 1211 Geneva 20, Switzerland Authorized officer

Olivia RANAIVOJAONA

Telephone No.: (41-22) 338.83.38



INTERNATIONAL SEARCH REPORT

(PCT Article 18 and Rules 43 and 44)

Applicant's or agent's file reference FOR FURTHER see Notification of Transmittal of International Search Report (Form PCT/ISA/220) as well as, where applicable, item 5 below.					
International application No.	International filing date (day/month/year)	(Earliest) Priority Date (day/month/year)			
PCT/GB 99/04156	09/12/1999	09/12/1998			
Applicant					
VECTURA LIMITED et al.					
This International Search Report has bee according to Article 18. A copy is being tra	n prepared by this International Searching Aut ansmitted to the International Bureau.	hority and is transmitted to the applicant			
This International Search Report consists It is also accompanied by	of a total of sheets. a copy of each prior art document cited in this	s report.			
Basis of the report					
	international search was carried out on the ba less otherwise indicated under this item.	sis of the international application in the			
the international search w Authority (Rule 23.1(b)).	vas carried out on the basis of a translation of	the international application furnished to this			
was carried out on the basis of th contained in the internation filed together with the internation furnished subsequently to	e sequence listing: onal application in written form. ernational application in computer readable for o this Authority in written form.	nternational application, the international search			
	o this Authority in computer readble form.	lose not go bayond the displayure in the			
	osequently furnished written sequence listing o is filed has been furnished.	ioes not go beyond the disclosure in the			
the statement that the info furnished	ormation recorded in computer readable form	is identical to the written sequence listing has been			
2. Certain claims were fou	nd unsearchable (See Box I).				
3. Unity of Invention is lac	king (see Box II).				
4. With regard to the title,					
the text is approved as su	ibmitted by the applicant.				
the text has been establis	hed by this Authority to read as follows:				
	abmitted by the applicant. Shed, according to Rule 38.2(b), by this Author Be date of mailing of this international search re				
6. The figure of the drawings to be publ	lished with the abstract is Figure No.	<u></u>			
as suggested by the appli	icant.	None of the figures.			
because the applicant fail	ed to suggest a figure.	_			
because this figure better	characterizes the invention.				

A. CLASSIFICATION OF SUBJECT MATTER IPC 7 A61K9/00 A61K9/14

A61K9/72

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols) IPC 7 A61K

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practical, search terms used)

WPI Data, PAJ, CHEM ABS Data

Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X	WO 97 03649 A (COORDINATED DRUG DEVELOPMENT LTD., GB) 6 February 1997 (1997-02-06) cited in the application claims 1-7,10,12-14,19,20,22-24,26,29,30,36 page 5, line 32 -page 6, line 9 page 7, line 38 -page 8, line 5 page 12, line 9 - line 18 page 13, line 8 - line 12 example 1	3,5, 7-15,26, 33,34, 36,37

X Further documents are listed in the continuation of box C.	Patent family members are listed in annex.
 Special categories of cited documents: "A" document defining the general state of the art which is not considered to be of particular relevance "E" earlier document but published on or after the international filing date "L" document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified) "O" document referring to an oral disclosure, use, exhibition or other means "P" document published prior to the international filing date but later than the priority date claimed 	"T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention "X" document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone "Y" document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art. "&" document member of the same patent family
Date of the actual completion of the international search	Date of mailing of the international search report
28 June 2000	04/07/2000
Name and mailing address of the ISA	Authorized officer
European Patent Office, P.B. 5818 Patentlaan 2 NL – 2280 HV Rijawijk Tel. (+31–70) 340–2040, Tx. 31 651 epo nl, Fax: (+31–70) 340–3016	Scarponi, U

INTERNATIONAL SEARCH REPORT

rnational Application No
PCT/GB 99/04156

Category *	ation) DOCUMENTS CONSIDERED TO BE RELEVANT Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
etegory *	Спалон от досинент, with видеалон, where appropriate, от the невозали разведее	
\ \	WO 96 32096 A (INHALE THERAPEUTIC SYSTEM,U.S.A.) 17 October 1996 (1996-10-17)	1,3,8, 11,16, 19,20, 25-28, 32,33,37
	claims figures example 4	
A	WO 96 23485 A (COORDINATED DRUG DEVELOPMENT LTD.,GB) 8 August 1996 (1996-08-08) cited in the application	1,3,8, 11,16, 19,20, 25-28, 32,33,37
	claims 	

1

INTERNATIONAL SEARCH REPORT

Information on patent family members

national Application No
PCT/GB 99/04156

Patent document cited in search report			Publication date		Patent family member(s)	Publication date	
WO	9703649	Α	06-02-1997	AU	6620396 A	18-02-1997	
	.,	• •		CA	2226657 A	06-02-1997	
				EP	0871430 A	21-10-1998	
				JP	11509546 T	24-08-1999	
WO	9632096	Α	17-10-1996	AU	706195 B	10-06-1999	
				AU	5550396 A	30-10-1996	
				CA	2218074 A	17-10-1996	
				ΕP	0820277 A	28-01-1998	
				JP	11501657 T	09-02-1999	
WO	9623485	Α	08-08-1996	AU	699131 B	26-11-1998	
				AU	4545696 A	21-08-1996	
				BG	101858 A	30-04-1998	
			•	BR	9607490 A	23-12-1997	
				CA	2211874 A	08-08-1996	
				CZ	9702443 A	14-01-1998	
				EP	0806938 A	19-11-1997	
				FI	973151 A	30-09-1997	
				HU	9802209 A	01-02-1999	
				JP	10513174 T	15-12-1998	
				NO	973502 A	30-09-1997	
				NZ	300654 A	25-02-1999	
				PL	321572 A	08-12-1997	
				SK	103697 A	14-01-1998	
				ZA	9600721 A	19-08-1996	

PCT

INTERNATIONAL PRELIMINARY EXAMINATION REPORT

(PCT Article 36 and Rule 70)

Applicant's	or age	nt's file reference		0 11-16	1 4 T (Mal - 6 later 1)
CAHJED:	3497	wo	FOR FURTHER ACTION		tion of Transmittal of International Examination Report (Form PCT/IPEA/416)
International application No.			International filing date (day/month	/year)	Priority date (day/month/year)
PCT/GB9	9/04	156	09/12/1999		09/12/1998
Internationa A61K9/00		nt Classification (IPC) or na	tional classification and IPC		
Applicant					
VECTUR.	A LIN	AITED et al.			
		ational preliminary exami smitted to the applicant a		by this Inter	national Preliminary Examining Authority
2. This F	REPO	RT consists of a total of	9 sheets, including this cover sh	neet.	
b€	en a	mended and are the bas		ontaining rec	, claims and/or drawings which have tifications made before this Authority PCT).
Thosa			0 -1		
rnese	ann	exes consist of a total of	9 sneets.		
					·
3. This re	eport	contains indications rela	iting to the following items:		
1	\boxtimes	Basis of the report			
		Priority			
511	\boxtimes	Non-establishment of o	pinion with regard to novelty, inv	entive step a	and industrial applicability
IV	\boxtimes	Lack of unity of invention			
v	☒		nder Article 35(2) with regard to i	novelty, inver	ntive step or industrial applicability;
VI		Certain documents cité	ed		
VII		Certain defects in the in	nternational application		
VIII	\boxtimes	Certain observations or	n the international application		
Date of sub	missio	on of the demand	Date of o	completion of the	his report
03/07/200	00		19.03.20	001	
	exam	g address of the international ining authority;	al Authoriz	ed officer	STATE OF STA
<u></u>	D-80	opean Patent Office 0298 Munich +49 89 2399 - 0 Tx: 523656	Bamin	ger, U	Land Land And And And And And And And And And A
		+49 89 2399 - 4465	· ·	ne No. +49.89	2399 2176



International application No. PCT/GB99/04156

I. B	asis	of t	the	repo	ort

1.	resp the	This report has been drawn on the basis of (substitute sheets which have been furnished to the receiving Office of the response to an invitation under Article 14 are referred to in this report as "originally filed" and are not annexed to the report since they do not contain amendments (Rules 70.16 and 70.17).): Description, pages:						
	1-5, 18-3	,7,9-16, 38	as originally file	d				
	6,8,	17,17a	as received on		06/12/2000	with letter of	30/11/2000	
	Clai	ims, No.:						
	1-38	3	as received on		06/12/2000	with letter of	30/11/2000	
2.	lang	With regard to the language , all the elements marked above were available or furnished to this Authority in the anguage in which the international application was filed, unless otherwise indicated under this item.						
	The	se elements were	available or furnis	shed to this Au	thority in the fo	ollowing language:	, which is:	
		the language of a	translation furnis	hed for the pu	rposes of the i	nternational searcl	h (under Rule 23.1(b)).	
		the language of p		-			, , , , , , , , , , , , , , , , , , , ,	
		the language of a 55.2 and/or 55.3).		hed for the pu	rposes of inter	national preliminar	ry examination (under Rule)
3.		n regard to any nu o rnational prelimina			•		ional application, the ing:	
		contained in the ir	nternational appli	cation in writte	n form:			
		filed together with	the international	application in	computer read	lable form.		
		furnished subsequ	uently to this Auth	nority in written	form.			
		furnished subsequ	uently to this Auth	nority in compu	iter readable fo	orm.		
		The statement that the international a				e listing does not q	go beyond the disclosure i	n
		The statement that listing has been for		recorded in co	omputer reada	ble form is identica	al to the written sequence	
4.	The	amendments hav	e resulted in the	cancellation of	:			
		the description,	pages:					
	\boxtimes	the claims,	Nos.:	39-40				
		the drawings,	sheets:					

INTERNATIONAL PRELIMINARY EXAMINATION REPORT

International application No. PCT/GB99/04156

5.		This report has been established as if (some of) the amendments had not been made, since they have been considered to go beyond the disclosure as filed (Rule 70.2(c)):
		(Any replacement sheet containing such amendments must be referred to under item 1 and annexed to this report.)
6.	Ado	ditional observations, if necessary:
III.	Nor	n-establishment of opinion with regard to novelty, inventive step and industrial applicability
1.		questions whether the claimed invention appears to be novel, to involve an inventive step (to be non- ious), or to be industrially applicable have not been examined in respect of:
		the entire international application.
	⊠	claims Nos. 31-38.
be	caus	se:
		the said international application, or the said claims Nos. relate to the following subject matter which does not require an international preliminary examination (<i>specify</i>):
	⊠	the description, claims or drawings (<i>indicate particular elements below</i>) or said claims Nos. 31-38 are so unclear that no meaningful opinion could be formed (<i>specify</i>): see separate sheet
		the claims, or said claims Nos. are so inadequately supported by the description that no meaningful opinion could be formed.
		no international search report has been established for the said claims Nos
2.	and	neaningful international preliminary examination report cannot be carried out due to the failure of the nucleotide Vor amino acid sequence listing to comply with the standard provided for in Annex C of the Administrative cructions:
		the written form has not been furnished or does not comply with the standard.
		the computer readable form has not been furnished or does not comply with the standard.
IV	. Lac	ck of unity of invention
1.	In r	esponse to the invitation to restrict or pay additional fees the applicant has:
		restricted the claims.
		paid additional fees.

INTERNATIONAL PRELIMINARY EXAMINATION REPORT

International application No. PCT/GB99/04156

		paid additional fees under protest.									
		neither restricted nor paid additional fees.									
2.	Ø	This Authority found that the requirement of unity of invention is not complied and chose, according to Rule 68.1, not to invite the applicant to restrict or pay additional fees.									
3.	This	This Authority considers that the requirement of unity of invention in accordance with Rules 13.1, 13.2 and 13.3 is									
		complied with.									
	⊠	not complied with for the see separate sheet	e followii	ng reasor	ns:						
4.		Consequently, the following parts of the international application were the subject of international preliminary examination in establishing this report:									
	Ø	all parts.									
		the parts relating to clair	ns Nos.								
V.		Reasoned statement under Article 35(2) with regard to novelty, inventive step or industrial applicability; itations and explanations supporting such statement									
1.	Stat	ement									
	Nov	relty (N)	Yes: No:	Claims Claims	1-30						
	Inve	entive step (IS)	Yes: No:	Claims Claims	1-23 24, 27- 29						
	Indu	ustrial applicability (IA)	Yes: No:	Claims Claims	1-38						

see separate sheet

2. Citations and explanations

VIII. Certain observations on the international application

The following observations on the clarity of the claims, description, and drawings or on the question whether the claims are fully supported by the description, are made: see separate sheet

Re Item I

Basis of the report

The corrections of the figures 200 and 500 to 20 and 50 on p. 8 line 23 of the description were found allowable, due to the statement on p. 8, lines 1-3 and the fact that the aspect ratios of the claimed sizes of the amino acid particles lie within or close to the new corrected values.

Re Item III

Non-establishment of opinion with regard to novelty, inventive step and industrial applicability

- 3.1 Present claim 31 of the application is unclear as to the subject-matter for which protection is sought (Art. 6 PCT). It claims particles of amino acid that are obtainable by a method of preparing particles of claims 1-6. The claim appears to contain a circle reference and is redundant and not clear to the extent that no meaningful opinion on the novelty and inventive step can be formed (Article 34(4)(a)(ii) PCT).
- 3.2 Due to the reference to claim 31, the same applies to the subject-matter of claims 32-35.
- Claims 36-38 of the present application refer to particles, a method and a powder "substantially as herein described". The term "substantially" is a very vague term in this context, since it does not clearly define the scope of the claims. To which extent is the subject-matter that of the preceding claims or the description? There is not sufficient support for the many thinkable particles, powders for inhalation and methods of producing these in the disclosure of the invention as filed. This renders the claims unclear to the extent that no meaningful opinion on the novelty and inventive step can be formed.

Re Item IV

Lack of unity of invention

As long as claims 24 and 27-29 (in so far as they refer to claim 24) do not refer back to the amino acids of claims 1-6, the present application addresses two different inventions, which cannot be considered to be linked by a single inventive concept (Rule 13.1, PCT). One invention aims at providing improved powders for dry powder inhalers by including specified amino acid particles, while the other invention aims at the production of amino acid particles in general. The proposed solutions do not possess the same or equivalent special technical features to characterise the contribution to the art.

Re Item V

Reasoned statement under Rule 66.2(a)(ii) with regard to novelty, inventive step or industrial applicability; citations and explanations supporting such statement

Reference is made to the following documents:

D1: WO 97 03649 A D2: WO 96 32096 A D3: WO 96 23485 A

- The subject-matter of claim 1 appears to be novel (Art. 33 (2) PCT) in view of the documents available to the examiner. Claim 1 has been understood as meaning "Amino acid particles in which a representative sample of the particles has a bulk density of ...". D1 and D3 both disclose isolated amino acid particles, however they do not explicitly disclose the bulk density of these particles (see also item 8.1).
- 5.2 The subject-matter of the independent claim 3 appears to be novel in view of the documents available to the examiner.
 - D1 (p. 9, lines 16-28; p.11, lines 33-36 and p.12, lines 5-8) explicitly discloses additive material that advantageously includes one or more compounds selected

EXAMINATION REPORT - SEPARATE SHEET

documents available to the examiner.

from amino acids (e.g. leucine). Preferably at least 90% by weight of the additive particles have a particle size (aerodynamic diameter) of less than 10 µm. A mass median aerodynamic diameter of not more than 5 µm is not explicitly or implicitly disclosed.

D2 (p. 5, line 25- p. 6, line 3; p. 4, lines 23-29 and example 4) discloses a powder of the relevant size, however the powder is produced by spray drying a homogenous aqueous mixture containing the active agent and additives. D2 does not disclose isolated amino acid particles of the relevant size.

- 5.3 The subject-matter of the independent claim 4 appears to be novel in view of the documents available to the examiner. D1 (p. 12, lines 10-11) and D3 (p.14, lines 24-25) both disclose "plate-like" amino acid particles, that can be seen as equivalent to the flakes of claim 5, however D1
 - The subject-matter of the independent claim 7 appears to be novel in view of the

and D3 do not explicitly disclose the thickness of these particles.

- The subject-matter of the independent claims 18-20 appear to be novel in view of the documents available to the examiner.
- The subject-matter of the independent claim 24 appears to be novel in view of the documents available to the examiner. D2 (p. 18, lines 17-23; p.19, lines 5-6 and ex. 4) disclose the preparation of a powder by spray drying of an aqueous solution that includes an amino acid. However no isolated amino acid particles are formed. The applicant is made aware that inevitably some sublimation of the amino acid will always take place when spray drying. This feature is therefore implicitly also present in D2.
- 5.7 For the purpose of examining the inventive step of the present application, D1 can be regarded as the closest prior art.
 - The problem to be solved appears to lie in the provision of an alternative powder, for use in dry powder inhalers, with good flow properties and a high respirable fraction that includes amino acid particles.
 - The solutions found in claims 1, 3 and 4 of the present application are to use "low-

EXAMINATION REPORT - SEPARATE SHEET

density amino acid" particles (see descr. p. 9, lines 16-20).

There is no indication in the prior art for a person skilled in the art to use amino acid particles with a bulk density, a MMAD or a flake thickness according to claims 1, 3 and 4 to reach this aim.

Therefore the subject-matters of claims 1, 3 and 4 can be considered inventive according to Art. 33 (3) PCT.

The same arguments apply to the independent claims 7 and 18.

The independent claims 19 and 20 refer to methods for the preparation of the amino acid particles as claimed in claims 1-6. As process, inevitably leading to the manufacture of a product that is new and inventive, claims 19 and 20 also fulfill the requirements Art. 33 (3) PCT.

For the independent claim 24 of the present application, the problem appears to lie in the provision of a method of producing amino acid particles. The solution according to claim 24 cannot be considered to involve an inventive step. As explained in point 5.6 above, the subject-matter of claim 24 differs with D2 only in the fact that D2 discloses the spray drying of a solution that includes an amino acid, but not exclusively, leading to particles that contain amino acids but not inevitably isolated amino acid particles (cf. D2, ex. 4). However it would be obvious to a person skilled in the art that this same method would also be suitable for producing isolated amino acid particles. Especially since the method of spray drying is very common in the art.

Re Item VIII

Certain observations on the international application

- The phrase "a sample of" in claims 1 and 2 renders the subject-matter of claims 1 8.1 and 2 unclear, since a sample is not in every case representative of substantially all the particles.
- 8.2 It is not made clear in claim 8 that the "active material" is intended to be biologically active (see descr. p. 21, lines 10-12). Without this clarification in the claim itself, the subject-matter of claim 8 can not be considered clear (PCT guidelines III-4.2).

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EXAMINATION REPORT - SEPARATE SHEET

- 8.3 The expression "at least some" in claim 24 is vague (PCT guidelines III-4.5).
- 8.4 Claims 28 and 29 lack clarity in that claim 3 of the application was amended to claim amino acid particles with a MMAD of not more than 5 µm. This amendment to claim 3 was however not carried on into claims 28 and 29, that still refer to amino acid particles with a MMAD of 10 µm, leading to inconsistency of claims 28 and 29 with some of the claims they refer to.

5

leucine having a low-density shows flow enhancing properties when added to powders. In particular, the addition of the low-density leucine to a powder gives improved glidant properties as well as improved anti-adherent properties.

Where reference is made to "density" in this specification, it is to be understood as being a reference to bulk density unless it is clear from the context that a different measurement of density is being referred to.

Advantageously, the amino acid particles have a bulk 10 density not more than $0.1~{\rm gcm}^{-3}$ and preferably not more than $0.05~{\rm gcm}^{-3}$.

The invention also provides amino acid powder, the powder having a bulk density of not more than 0.1 gcm⁻³.

A second aspect of the invention provides amino acid

15 particles having a mass median aerodynamic diameter (MMAD) of

not more than 5µm. Reference is made above to the MMAD of

the particles. Where the particles have a low bulk density

in accordance with the first aspect of the invention, the

actual diameter of the particles can be relatively large

20 while the MMAD is still small enough for the desired

aerodynamic characteristics of the particles.

Alternatively, the size distribution of the particles can be characterised by their volume mean diameter (VMD). Advantageously, the VMD of the amino acid particles is not more than $10\,\mu\text{m}$, preferably not more than $5\,\mu\text{m}$.

In some cases, the particles of the third aspect of the invention will also have the desired MMAD (or VMD) of the second aspect of the invention.

It has been found that the thin flakes of leucine in accordance with this further aspect of the invention generally have a low density and improved flow properties.

It has been found to be particularly advantageous for the leucine to be in the form of flakes having a thickness of less than about 100nm.

It has been found that when, for example, the leucine flakes have been prepared using the spray drying method described below, that they have a very small thickness of less than 100nm and a relatively large width. It has been found that the flakes may become fractured during subsequent processing of the powder but that the beneficial properties of the flakes are not substantially diminished. It is thought, therefore, that it is the very small thickness of the flakes which gives their advantageous properties.

The aspect ratio of the flakes of amino acid can be

20 considered to be the (width of the particles)/(thickness of
the particles). Advantageously the aspect ratio of the
particles is at least 20, preferably at least 50.

Observation of the thickness of the flakes may be made
by studying electron microscope (SEM) images of the
25 particles. For example, flakes may be mounted on an electron

and the temperature required to form a vapour of that amino acid.

According to a further aspect of the invention, in the method of producing particles of amino acid, droplets of

5 amino acid in a solvent are dried in a spray drying step to form solid particles of amino acid, the method being such that at least some of the amino acid sublimes during the spray drying.

Advantageously, the method includes the step of spray 10 drying amino acid in a solvent.

Advantageously, the material to be dried comprises amino acid in solution, which is advantageously an aqueous solution.

Where the amino acid is one which sublimes, for example

leucine, it is thought that it may be advantageous for some

sublimation of the leucine to take place during the spray

drying of the leucine to give the most advantageous

morphology of the leucine particles produced. In such a

case, advantageously, the spray drying method is such that at

least some of the amino acid sublimes during the spray

drying.

Conventional spray drying of the amino acid may produce large particles of amino acid which are generally spherical in shape. Where the amino acid is leucine, such particles may have a particle diameter of 40µm or more. Such leucine particles produced by a spray drying method are described in

Pharmaceutica Acta Helvetiae 70(1995) 133-139. Such

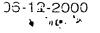


Claims:

- 1. Amino acid particles in which a sample of the particles has a bulk density not more than 0.1 gcm⁻³.
- 5 2. Amino acid particles according to claim 1, in which a sample of the particles has a bulk density not more than 0.05 gcm⁻³.
 - 3. Amino acid particles having a mass median aerodynamic diameter (MMAD) not more than $5\mu m$.
- 10 4. Amino acid particles being in the form of flakes having a thickness of not more than $0.5\mu m$.
 - 5. Amino acid particles according to claim 4 in which the flakes have a thickness of not more than 100nm.
- Amino acid particles according to any preceding claim,
 in which the amino acid is leucine.
 - 7. A powder for use in a dry powder inhaler, the powder including active material and amino acid particles according to any of claims 1 to 6.
- 8. A powder according to claim 7, in which the powder
 20 includes not more than 20% by weight of amino acid based on
 the weight of the powder.
 - 9. A power according to claim 8, in which the powder includes not more than 10% by weight of amino acid based on the weight of the powder.
- 25 10. A powder according to claim 7 or claim 8, the powder further including particles of a diluent.

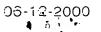
AMENDED SHEET

- 11. A powder according to claim 10, in which the diluent includes a crystalline sugar.
- 12. A powder according to claim 10 or claim 11, in which the diluent has a particle size such that at least 90% by weight of the diluent particles have a particle size not more than $10\mu m$.
- 13. A powder according to claim 10 or claim 11, in which the diluent has a particle size such that at least 90% by weight of the diluent particles have a particles size not 10 less than 50μm.
- 14. A powder according to claim 10 or claim 11, in which the diluent has a fine particle portion having a particle size such that at least 90% by weight of the particle of the fine particle portion have a particle size not more than 10μm and a coarse particle portion having a particle size such that at least 90% by weight of the particles of the coarse particle portion have a particle size not less than 50μm.
- 15. A powder according to claim 14, in which the fine particle portion and coarse particle portion comprise the 20 same material.
 - 16. A powder according to any of claims 14 or 15, in which the powder includes not more than 5% by weight of the fine particle portion based on the weight of the powder.



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- 17. A powder according to any of claims 14 to 16, in which the powder includes not more than 95% by weight of the coarse particle portion based on the weight of the powder.
- 18. A dry powder inhaler, the inhaler containing powder according to any of claims 7 to 17.
- 19. A method of preparing particles of amino acid as claimed in any of claims 1 to 6, the method including the step of forming solid amino acid particles from a vapour or from a solvent, the method being such that the particles are formed while being suspended in a gas flow.
 - 20. A method of preparing particles of amino acid as claimed in any of claims 1 to 6, the method including the step of condensing amino acid vapour to form solid amino acid particles.
- 15 21. A method according to claim 19 or claim 20, in which particles of amino acid are formed by aerosol condensation.
 - 22. A method according to claim 20 or claim 21, in which the method includes the steps of
 - a) heating the amino acid so that the amino acid formsa vapour;
 - b) mixing the amino acid vapour with cool air to form a cloud of condensed amino acid particles; and
 - c) collecting the condensed particles.
- 23. A method according to any of claims 20 to 22, the method
 25 including the step of heating the amino acid particles to a temperature of at least 150°C at ambient pressure.



- 24. A method of producing particles of amino acid, in which droplets of amino acid in a solvent are dried in a spray drying step to form solid particles of amino acid, the method being such that at least some of the amino acid sublimes during the spray drying.
 - 25. A method according to claim 19, in which the method includes the step of spray drying to form solid particles of amino acid.
- 26. A method according to claim 25, in which the material to 10 be dried comprises amino acid in solution.
 - 27. A method according to claim 24 or claim 26, in which material to be dried comprises amino acid in aqueous solution.
- 28. A method according to any of claims 24 to 27 in which 15 the droplets dried have a mean size of not more than $10\mu m$.
 - 29. A method according to any of claims 19 to 28, in which the method is such that the MMAD of the solid amino acid particles produced is not more than $10\mu m$.
- 30. A method according to claim 24, the method being such 20 that the amino acid particles produced are amino acid particles according to any of claims 1 to 6.
 - 31. Particles of amino acid obtainable by a method according to any of claims 19 to 29.
- 32. A method of making a powder according to any of claims 7 to 17, the method including the steps of mixing amino acid



according to any of claims 1 to 6 or claim 31 with active material.

- 33. A method of making a powder according to any of claims
 10 to 17, the method including the step of mixing amino acid
 5 according to any of claims 1 to 6 or claim 31 with active
 material followed by the step of mixing the amino acid and
 active material with a diluent.
- 34. Use of particles of amino acid according to any of claims 1 to 6 or claim 31 in a powder to improve the flow 10 properties of the powder.
 - 35. Use of particles of amino acid according to any of claims 1 to 6 or claim 31 in a powder for use in a dry powder inhaler.
- 36. Particles of amino acid being substantially as herein 15 described.
 - 37. A method of producing particles of amino acid, the method being substantially as herein described.
 - 38. A powder for inhalation, the powder being substantially as herein described.

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spray drying. The amino acid particles have a bulk densi not more than 10 μ m or are in the form of flakes having	formed ty of ne	from an amino acid vapour, for example by aerosol condensation, or to the more than 0.1 gcm ⁻³ or have a mass median aerodynamic diameter kness of not more than 100 μ m. The inclusion of the particles of amin improve the respirable fraction of the active material in the powder.			

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Improvements in or relating to Powders

This invention relates to particles for use in powders.

In particular, but not exclusively, the invention relates to

particles for use in powder compositions for dry powder

inhalers, especially particles of an amino acid for use in

such powders.

Inhalers are well known devices for administering pharmaceutical products to the respiratory tract by

10 inhalation. Inhalers are widely used particularly in the treatment of diseases of the respiratory tract.

There are a number of types of inhaler currently available. One device is the dry powder inhaler. The delivery of dry powder particles of pharmaceutical products

15 to the respiratory tract presents certain problems. The inhaler should deliver the maximum possible proportion of the active particles expelled to the lungs, including a significant proportion to the lower lung, preferably at the low inhalation capabilities to which some patients,

20 especially asthmatics, are limited. It has been found however, that, when currently available dry powder inhaler devices are used, in many cases only about 10% of the active particles that leave the device on inhalation are deposited in the lower lung. More efficient dry powder inhalers would

25 give clinical benefits.

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The physical properties of the powder used in the inhaler affect both the efficiency and reproducibility of delivery of the active particles and the site of deposition in the respiratory tract.

5 On exit from the inhaler device, the active particles should form a physically and chemically stable aerocolloid which remains in suspension until it reaches a conducting bronchiole of smaller branching of the pulmonary tree or other absorption site preferably in the lower lung. Once at the absorption site, the active particle should be capable of efficient collection by the pulmonary mucosa with no active particles being exhaled from the absorption site.

The size of the active particles is particularly important. For effective delivery of active particles deep 15 into the lungs, the active particles should be small, with an equivalent aerodynamic diameter substantially in the range of 0.1 to 5 µm, approximately spherical and monodispersed in the respiratory tract. Small particles are, however, thermodynamically unstable due to their high surface area to 20 volume ratio, which provides significant excess surface free energy and encourages particles to agglomerate. In the inhaler, agglomeration of small particles and adherence of particles to the walls of the inhaler are problems that result in the active particles leaving the inhaler as large 25 stable agglomerates or being unable to leave the inhaler and remaining adhered to the interior of the inhaler.

The uncertainty as to the extent of formation of stable agglomerates of the particles between each actuation of the inhaler and also between different inhalers and different batches of particles leads to poor dose reproducibility.

Some known dry powders for use in dry powder inhalers include carrier particles to which the fine active particles adhere whilst in the inhaler device, but which are dispersed from the surfaces of the carrier particles on inhalation into the respiratory tract to give a fine suspension. The carrier particles are often large particles greater than 90 µm in diameter to give good flow properties as indicated above.

Small particles with a diameter of less than 10µm may be deposited on the wall of the delivery device and have poor flow and entrainment properties leading to poor dose uniformity.

The increased efficiency of redispersion of the fine active particles from the agglomerates or from the surfaces of carrier particles during inhalation is regarded as a critical step in improving the efficiency of the dry powder inhalers.

In some dry powder inhaler devices, doses of powder containing only active particles are dispensed. The powder contains no carrier particles or other additives and the amount of powder in each dose is small, usually less than

1mg. The volume of the dose may be, for example, approximately $6.5\mu l$.

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Problems involved in dispensing a powder containing only particles of active material include

- i. formation of stable agglomerates of the small particles which often are not broken down into individual particles in the air stream when the particles are inhaled and are, therefore, less likely to reach the lower lung on inhalation of the powder than the fine individual active particles;
 - ii. variation in the amount of powder metered from a reservoir of the inhalation device due to poor flow properties of the powder and inconsistent agglomeration, leading to inconsistency in the size of dose, which may vary as much as ± 50% compared with the nominal dose for the device;
 - iii. incomplete removal of the dose from the device due to adherence of the particles to the walls of the device, leading to poor dose reproducibility.
- In order to increase the proportion of active particles which may be delivered to the lung, it has been proposed to add a further component to the powder.

WO96/23485 describes the addition of an additive material to a powder for inhalation including carrier particles and active particles to improve the respirable

fraction of the active material. A preferred additive material is leucine.

W097/03649 also describes the addition of leucine to powder compositions for dry powder inhalers, in which the compositions do not include carrier particles.

While the addition of the additive material to the compositions described in WO96/23485 and WO97/03649 give improved respirable fractions of the active components, it would clearly be desirable to make the effect of the additive material still more beneficial.

According to the invention there are provided amino acid particles in which a sample of the particles has a bulk density not more than $0.1~{\rm gcm}^{-3}$.

The bulk density of the sample may be determined using the test described below.

The amino acid particles may comprise one amino acid or a mixture of two or more amino acids. Preferred amino acids include those amino acids which sublime, in particular leucine and iso-leucine, and also alanine, valine, serine and phenyl alanine.

An especially preferred amino acid is leucine.

The bulk density of standard crystalline leucine currently available is in the range of 0.6 to 0.7 gcm⁻³ and the bulk density of leucine that has been milled is in the range of 0.3 to 0.4 gcm⁻³. The leucine in accordance with the invention has very low bulk density. It has been found that

leucine having a low-density shows flow enhancing properties when added to powders. In particular, the addition of the low-density leucine to a powder gives improved glidant properties as well as improved anti-adherent properties.

Where reference is made to "density" in this specification, it is to be understood as being a reference to bulk density unless it is clear from the context that a different measurement of density is being referred to.

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Advantageously, the amino acid particles have a bulk 10 density not more than $0.1~{\rm gcm}^{-3}$ and preferably not more than $0.05~{\rm gcm}^{-3}$.

The invention also provides amino acid powder, the powder having a bulk density of not more than 0.1 gcm⁻³.

A second aspect of the invention provides amino acid

particles having a mass median aerodynamic diameter (MMAD) of

not more than 10μm. Preferably, the MMAD is not more than

5μm. Reference is made above to the MMAD of the particles.

Where the particles have a low bulk density in accordance

with the first aspect of the invention, the actual diameter

of the particles can be relatively large while the MMAD is

still small enough for the desired aerodynamic

characteristics of the particles.

Alternatively, the size distribution of the particles can be characterised by their volume mean diameter (VMD).

25 Advantageously, the VMD of the amino acid particles is not

more than $10\mu\text{m}$, preferably not more than $5\mu\text{m}$.

As indicated above, it has been found that a particularly preferred amino acid is leucine.

It has been found that leucine having a VMD of less than 10µm has improved flow properties when added to powders. It is thought that the small particle size of the leucine is closely associated with a low bulk density. As described above, such particles give improved flow properties.

Advantageously, the amino acid particles have a volume mean diameter not more than 5µm. That size is very small for amino acid particles, in particular leucine particles.

In a third aspect of the invention, there is provided amino acid particles being in the form of flakes having a thickness of not more than 0.5 μ m. Preferably the flakes have a thickness of not more than 100nm.

As indicated above, a preferred amino acid is leucine.

Conventional leucine is in the form of flakes having a

thickness of at least 1μm and usually greater than 5μm. It

has been found that, by reducing the thickness of the flakes,

the flow properties of the leucine particles is improved. It

20 is thought that when the leucine is added to a powder the

thin leucine flakes act as "spacers" between the particles of

the powder which improves its flow properties, in particular

the glidant properties.

In some cases, the particles of the third aspect of the invention will also have the desired MMAD (or VMD) of the second aspect of the invention.

It has been found that the thin flakes of leucine in accordance with this further aspect of the invention generally have a low density and improved flow properties.

It has been found to be particularly advantageous for the leucine to be in the form of flakes having a thickness of less than about 100nm.

It has been found that when, for example, the leucine flakes have been prepared using the spray drying method described below, that they have a very small thickness of less than 100nm and a relatively large width. It has been found that the flakes may become fractured during subsequent processing of the powder but that the beneficial properties of the flakes are not substantially diminished. It is thought, therefore, that it is the very small thickness of the flakes which gives their advantageous properties.

The aspect ratio of the flakes of amino acid can be

20 considered to be the (width of the particles)/(thickness of
the particles). Advantageously the aspect ratio of the
particles is at least 200, preferably at least 500.

Observation of the thickness of the flakes may be made by studying electron microscope (SEM) images of the 25 particles. For example, flakes may be mounted on an electron microscope stub with double sided tape and coated with gold prior to examination on an electron microscope.

An alternative method for observing the dimensions of particles of the present invention is by sizing the particles on a microscope slide in a similar way to that described in British Pharmacopoeia 1973 (page 645, Ergotamine Aerosol Inhalation). In this case a small quantity of particles, for example 10 to 100mg, are dropped onto a microscope slide and examined under a microscope to assess the particle size of the deposit.

Where reference is made above to the shape and size of the particles, it should be understood that the reference is to the shape and size of the individual particles. Those particles may become agglomerated to form clusters of individual particles.

The amino acid of the first, second and third aspects of the invention will all be referred to below as "low-density amino acid" for ease of reference. Furthermore, where the amino acid is, for example, leucine, it will be referred to below as "low-density leucine". It should be understood, however, that the amino acid of the second and third aspects of the invention, for example, might not have the bulk density required in respect of the first aspect of the invention.

Where the amino acid is leucine, advantageously, the leucine is L-leucine. L-leucine is a naturally occurring

form of leucine and is therefore preferred when the leucine is to be used in pharmaceutical compositions or other compositions that may enter the body.

Advantageously, the particles of low-density amino acid include no further materials other than the amino acid. The particles may include a mixture of more than one amino acid.

According to the invention there is also provided a powder for use in a dry powder inhaler, the powder including active material and low-density amino acid particles.

10 The low-density amino acid is particularly advantageous for use in a powder for inhalation. There are several conventional additives that are included in powder compositions for inhalation to improve the flow properties of the powder. Many of the flow enhancing additives are,

15 however, undesirable for inhalation because they are not particularly physiologically acceptable, for example silica.

Amino acids are bio-compatible and relatively safe for

inhalation.

It has been found that the addition of the low-density
amino acid to a powder for inhalation can give an improved
respirable fraction for the powder and/or improved emptying
of the powder from the inhaler device on actuation of the
inhaler.

Advantageously, the powder includes not more than 10% 25 by weight of low-density amino acid based on the weight of the powder. For powders for inhalation, where the low

density amino acid is added to the powder to improve the dispersal of the active particles, it has been found that while the addition of up to 10% by weight of the low-density amino acid can give improved powder performance, on the addition of about 20% by weight of the low-density amino acid, the benefit was reduced.

Where the low-density amino acid is used as a flow aid, for example in powders other than for use in dry powder inhalers, it has been found that the low-density amino acid can be included in greater amounts without detrimental effects, for example the low-density amino acid may be present at a % by weight of 50%.

As indicated above, in some powders for inhalation, active material comprises substantially all of the powder.

15 In some cases a small amount of additives, for example colorants and flavourings are included. Thus, the powder may include less than 10%, preferably less than 5% by weight of materials other than the active material and the amino acid, based on the weight of the powder. The active material may comprise not less than 60% by weight of the powder.

In other powders for inhalation, the powder includes other diluents, for example carrier particles as described above. Thus, the powder may further include particles of a diluent. The carrier particles may be present in an amount of at least 50%, preferably at least 90%, more preferably at least 95%, by weight based on the weight of the powder.

The diluent may have a particle size such that at least 90% by weight of the diluent particles have a particle size not more than $10\mu m$. It has been found that the addition of fine particles of diluent gives improved respirable fraction.

Alternatively, the diluent may have a particle size such that at least 90% by weight of the diluent particles have a particle size not less than $50\mu m$. Such particles are equivalent to the carrier particles described above and give improved flow properties to the powder.

It has been found that the addition of low-density amino acid gives improved respirable fraction of active particles when the powder is used in a dry powder inhaler. That is thought to be due to the improved flow properties of the powder leading to improved emptying of the powder from the inhaler device and/or improved dispersion of the active particles on actuation of the inhaler device.

Advantageously, the diluent has a fine particle portion having a particle size such that at least 90% by weight of the particle of the fine particle portion have a particle size not more than 10μm and a coarse particle portion having a particle size such that at least 90% by weight of the particles have a particle size not less than 50μm.

It will be understood that, unless it is clear to the contrary, the particle size or the diameter of the particles

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referred to is the aerodynamic diameter of the particles MMAD which may be measured by the method indicated below.

The fine particle portion and coarse particle portion may comprise the same material or different materials.

5 Furthermore, each of the fine particle portion and the coarse particle portion may comprise a mixture of more than one material.

The fine particle portion and the coarse particle portion may be, for example, simply mixed together. However, where the fine particle portion and the coarse particle portion comprise the same material, the diluent is advantageously prepared by treating coarse particles of the diluent to dislodge small fragments from their surfaces. The small fragments form the fine particle portion. Such a treatment may be carried out, for example, by careful milling of the coarse particles. Such treatment of the diluent particles is described, for example in WO96/23485.

The diluent particles may be composed of any pharmacologically inert material or combination of materials which is acceptable for inhalation. Advantageously, the diluent particles are composed of one or more crystalline sugars; the diluent particles may be composed of one or more sugar alcohols or polyols. Preferably, the diluent particles are particles of lactose.

Advantageously, the powder includes not more than 10%, preferably not more than 5% by weight of the fine particle

portion based on the weight of the powder. The fine particle portion of the diluent has a particle size that is advantageous for the delivery of the particles of the deep lung. It is generally advantageous for as little as possible of materials other than the active material to be transported to the deep lung.

According to the invention, there is also provided, a dry powder inhaler, the inhaler containing powder as described above.

- The present invention also provides a method of preparing particles of amino acid, the method including the step of forming solid amino acid particles from a vapour or from a solvent, the method being such that the particles are formed while being suspended in a gas flow.
- As indicated above, a conventional method of preparing amino acid, in particular leucine having a small particle size, is by milling the amino acid. Many amino acids, for example leucine are, however, soft materials and it is difficult to prepare leucine having a very small particle size in that way. Furthermore, the preparation of amino acid, for example leucine, using a milling technique increases the risk that there are contaminants or impurities in the amino acid. Furthermore, controlling the physical properties of powder produced by milling is difficult.
- 25 By preparing the amino acid by, for example, condensation from a vapour or by drying droplets of a solvent

containing leucine, particles of amino acid having a small particle size can be more easily obtained. Furthermore, greater control of particle size and morphology is possible. The particles are produced in suspended form, reducing the risk of contamination. The particles produced suspended in a gas flow may be easily classified and separated by their aerodynamic properties.

The method of producing particles of the amino acid in accordance with the invention will depend on the physical

10 nature of the amino acid. For example, leucine is an amino acid which sublimes and in one advantageous embodiment of the invention, leucine is condensed from leucine vapour to form the low-density particles according to the invention. Other amino acids decompose on heating. Such amino acids are

15 therefore not suitable to be condensed from their vapour but may, for example, be prepared by spray drying in accordance with a further embodiment of the invention to form low density amino acid.

Advantageously, the amino acid is a material which 20 sublimes.

In one aspect of the invention, the method of producing particles of amino acid includes the step of condensing amino acid vapour to form solid amino acid particles. That method is particularly desirable where the amino acid is to be co
25 condensed with another material. For example, where the amino acid is to be used in a powder including active

material, the amino acid and the active material may be cocondensed together.

Advantageously, the particles of amino acid are formed by aerosol condensation. One amino acid which is

5 particularly suited to preparation by that method is leucine.

Leucine sublimes at a temperature of about 220°C.

The method advantageously includes the steps of

- a) heating an amino acid so that the amino acid forms amino acid vapour;
- 10 b) mixing the amino acid vapour with cool air to form a cloud of condensed amino acid particles; and
 - c) collecting the condensed particles.

Advantageously, the amino acid is passed through a furnace. The furnace may be a tube furnace. The initial

15 amino acid particles are advantageously suspended from a fluidised bed by a flow of air. The material may then be carried in the gas flow into the tube furnace where it forms a vapour.

The condensed particles are advantageously collected in 20 a cyclone and/or a filter or by precipitation.

Advantageously, the method includes the step of heating the amino acid particles to a temperature of at least 150°C at ambient pressure. It is envisaged that the pressure could be reduced to reduce the temperature required to form the 25 amino acid vapour. The temperature to which the amino acid is heated will depend on the nature of the amino acid used

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and the temperature required to form a vapour of that amino acid.

According to a further aspect of the invention, in the method of producing particles of amino acid, droplets of

5 amino acid in a solvent are dried to form solid particles of amino acid.

Advantageously, the method includes the step of spray drying amino acid in a solvent.

Advantageously, the material to be dried comprises amino 10 acid in solution, which is advantageously an aqueous solution.

Where the amino acid is one which sublimes, for example leucine, it is thought that it may be advantageous for some sublimation of the leucine to take place during the spray drying of the leucine to give the most advantageous morphology of the leucine particles produced. In such a case, advantageously, the spray drying method is such that at least some of the amino acid sublimes during the spray drying.

20 Conventional spray drying of the amino acid may produce large particles of amino acid which are generally spherical in shape. Where the amino acid is leucine, such particles may have a particle diameter of 40μm or more. Such leucine particles produced by a spray drying method are described in 25 Pharmaceutica Acta Helvetiae 70(1995) 133-139. Such

particles have been found to be undesirable in that they do not give the desired properties for the low-density leucine.

Yamashita et al (Respiratory Drug Delivery J1 1998 p483)

describes the use of spray-dried L-isoleucine particles as a

5 hydrophobic carrier for inhalation. As indicated above,

conventional spray drying of an amino acid is thought to

produce particles having an undesirable morphology. The

conventional spray dried particles would, however, have the

properties desired in Yamashita having regard to the

10 consideration of hygroscopicity.

WO 98/31346 describes the spray drying of materials for inhalation. The spray drying is said to diminish the tap density of the material by increasing particle surface irregularities and increasing particle porosity. As

15 indicated above, it is believed that generally spherical porous particles do not give the desired properties for the materials of the present invention. In accordance with an aspect of the present invention, it has been found, surprisingly, that the herein described, unconventional,

20 spray drying of an amino acid gives particles having a new and particularly desirable morphology.

To give the best properties for the leucine and other amino acids produced by spray drying, it has been found that the droplet size is advantageously very small. The droplet size used in Pharmaceutica Acta Helvetiae 70(1995) 133-139 is at least 30µm. Most advantageously, the droplets dried in

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the method of the present invention have a mean size of not more than $10\mu m$, more preferably, not more than $5\mu m$.

It is also believed that a high temperature for the spray drying is of importance. In many cases, the

5 temperature of the spray drying for the formation of advantageous particles in accordance with at least one aspect of the present invention will be significantly greater than that used in conventional spray drying techniques. For example, the inlet air temperature of the spray dryer may be

10 greater than 150°C, preferably greater than 200°C at ambient pressure. The temperature of spray drying is of particular importance for materials which sublime and then condense to form the desired particle morphology. In such cases, advantageously the spray drying conditions are such that the 15 desired sublimation takes place, at least of part of the material, in the spray drying.

For both the first and second aspects of the invention in respect of the method, advantageously the method is such that the MMAD of the solid amino acid particles produced is not more than 10µm. As indicated above, amino acid particles having a small particle size can be used as an additive to improve the flow properties of powders.

Advantageously, the method is such that the amino acid particles produced are low-density amino acid particles as described above.

The invention also provides amino acid obtainable by a method as described above.

For ease of reference, the amino acid particles prepared by a method as described above will also be referred to as

5 "low-density amino acid". Also, where the low-density amino acid comprises, for example, leucine, the material will be referred to a "low-density leucine". It should be appreciated, however, that the amino acid produced by the methods might not have, for example, the bulk density

10 required in respect of the first aspect of the invention relating to the amino acid particles described above.

According to the invention, there is also provided a method of making a powder, the method including the steps of mixing low-density amino acid with active material.

As indicated above, the powder for may also include a diluent. In that case, advantageously, the method of producing the powder includes the step of mixing the low-density amino acid with active material followed by the step of mixing the low-density amino acid and active material with the diluent.

According to the invention, there is also provided the use of low-density amino acid in a powder to improve the flow properties of the powder.

Also provided is the use of low-density amino acid in a 25 powder for use in a dry powder inhaler.

As indicated above, the use of the amino acid can improve the respirable fraction of the active material in the It is thought that the respirable fraction is improved due to the improved dispersion of active material on 5 actuation of the inhaler. Furthermore, where the powder also includes carrier particles, it is thought that the lowdensity amino acid promotes the release of the active particles from the surfaces of the carrier particles on actuation of the inhaler.

10

The active material referred to throughout the specification will be material comprising one or a mixture of pharmaceutical products. It will be understood that the term "active material" includes material that is biologically active, in the sense that it is able to decrease or increase 15 the rate of a process in a biological environment. pharmaceutical products include those products that are usually administered orally by inhalation for the treatment of disease such as respiratory disease, for example β agonists, salbutamol and its salts or salmeterol and its 20 salts. Other pharmaceutical products which could be administered using a dry powder inhaler include peptides and polypeptides such as DNase, leucotrienes and insulin.

The active material may include a β_2 -agonist, which may include salbutamol a salt of salbutamol or a combination 25 thereof. Salbutamol and its salts are widely used in the treatment of respiratory disease. The active material may be salbutamol sulphate. The active material may be terbutaline, a salt of terbutaline, for example terbutaline sulphate, or a combination thereof. The active material may be ipatropium bromide.

The active material may include a steroid, which may be beclomethasone dipropionate or may be fluticasone. The active material may include a cromone, which may be sodium cromoglycate or nedocromil or its salts. The active material may include a leukotriene receptor antagonist.

The active material may include a carbohydrate, for example heparin.

Bulk Density

5

The bulk density (or poured density) of a material of the present invention is determined by the following method:

2g of the material is poured from weighing paper into a 100 cm³ graduated glass measuring cylinder in an upright position. Transfer of the material from the paper into the cylinder is made as rapidly as flow permits. The volume occupied by the poured powder in the cylinder is measured to the nearest 0.5 ml (bulk volume) and the weight of the powder is determined.

The bulk density of the material is calculated as the weight of the powder divided by the bulk volume.

An alternative method of measuring the bulk density is described in the European Pharmacopoeia 1997 2.9.15.

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Particle Size Distribution

The particle size distribution was determined by low angle laser light scattering (Mastersizer X, Malvern

5 Instruments, Malvern, UK). To approximately 5 mg of the sample to be analysed 10ml of dispersant was added (0.05% lecithin in cyclohexane). The sample suspension was sonicated for 30 seconds before analysis. The volume median diameter (VMD) and D(v,90) were determined. VMD is the

10 diameter such that 50% of the particles by volume have a diameter less than the VMD. D(v,90) is the equivalent volume diameter at 90% cumulative volume.

Mass Median Aerodynamic Diameter (MMAD)

15 The MMAD of particles of a material of the present invention is determined using Multi-Stage Liquid Impinger in accordance with the method described in European Pharmacopoeia (supplement 1999) 2.9.18. (Aerodynamic assessment of fine particles) for powder inhalers.

20

Embodiments for the invention will now be described by way of example.

Example 1

Spray-dried leucine was prepared by the following method.

L-leucine was spray-dried using a laboratory scale cocurrent spray-dryer (Model 191, Büchi, Switzerland). A
solution of 1.0 % w/w L-leucine in water was prepared and
atomised at a rate of 4.5 ml min⁻¹ using compressed air (600
1 hr⁻¹, 0.7mm nozzle). The droplets produced in the spraydryer had a VMD of not more than about 10µm. The inlet and
outlet air temperatures of the spray dryer were 220°C and
150°C respectively.

The resulting powder was collected by cyclone separation transferred to glass vials and stored in a desiccator at room temperature over silica gel until used. The spray-dried L-leucine was a light, loose white powder. A microscopic examination of the spray-dried powder showed the presence of thin, flake-like particles.

The bulk density and particle size diameter (as VMD) were determined for the spray-dried leucine. Bulk density and VMD were determined by the method indicated above.

Table 1 shows the bulk density and particle size distribution for unprocessed L-leucine and for 5 batches of L-leucine spray-dried by the method of Example 1. It will be seen that the spray-dried leucine had bulk densities in the range 0.02 g cm⁻³ to 0.05 g cm⁻³.

Table 1

Sample of L-leucine	Bulk Density (g cm ⁻³)	VMD (µm)	D(v,90)*	
unprocessed	0.710	ND	ND	
spray-dried A	0.042	4.2	10.6	
spray-dried B	0.035	ND	ND	
spray-dried C	0.029	ND	ND	
spray-dried D	0.035	ND	ND	
spray-dried E	0.032	3.9	11.9	

5 ND - Not Determined

* D(v,90) is the diameter below which 90% of particles by volume reside.

Flow Properties

The flow properties of the L-leucine were determined by measuring the Carr's Index of the powder. Spray-dried L-leucine was added to a powdered protein (BSA-maltodextrin 50:50).

Carr's Index of a sample was determined by measuring the volume (V_{pour}) of weight (W) poured into a 250 cm³ measuring cylinder and tapping the cylinder to obtain constant volume of the sample (V_{tap}). The poured density (bulk density) and the tap density are calculated as W/ V_{pour} and W/ V_{tap}

respectively and Carr's Index is calculated from the tapped density and the poured density by the formula

5 Table 2 shows the poured density (bulk density), tapped density and Carr's Index.

Table 2

	T				
Sample	Poured Density (gcm ⁻³)	Tapped Density (gcm ⁻³)	Carr's Index (%)		
	0.710	0.770	8.5		
unprocessed L-leucine	0.710	0.770	0.5		
spray-dried L-leucine	0.043	0.055	21.8		
BSA- maltodextrin (50:50)	0.240	0.540	55.5		
BSA- maltodextrin (50:50) + spray-dried L-leucine	0.093	0.146	36.0		

10

The addition of the spray-dried leucine to the protein powder gives a lower Carr's Index indicating improved flow properties.

15 Example 2

Aerosolised leucine was prepared by the following method.

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Ground L-leucine was passed through a tube furnace. The L-leucine particles were suspended from a fluidised bed by a flow of air (about 20 l min⁻¹). The particles were carried in a gas flow into the tube furnace, which was at a temperature ranging from 150 to 300°C. The material sublimed. The vapour emitted from the furnace was mixed with cool air giving a cloud of condensed particles that were subsequently collected in a cyclone and membrane filter. The material collected was light and "fluffy" and includes particles in the form of thin flakes.

The bulk density and particle size distribution were determined by the methods described in respect of Example 1 above, and are given in Table 3.

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Table 3

Sample of L-leucine	Bulk Density (gcm ⁻³)
unprocessed	0.70
milled (VMD = 18μ m)	0.30
condensed	0.04

5

Twin Stage Impinger

Powder blends were tested in a twin stage impinger (TSI)

(European Pharmacopoeia 1997 2.9.18) to assess the efficiency

10 of the delivery of the active particles to the lungs of a

patient by an inhaler device.

The TSI is a two-stage separation device used in the assessment of oral inhalation devices. Stage one of the apparatus including the upper impinger is a simulation of the upper respiratory tract. Stage two which includes the lower impinger is a simulation of the lower respiratory tract.

The liquid used in both the upper and lower impinger is distilled water for the examples below.

In use, the inhaler is placed in a mouth of the TSI.

20 Air is caused to flow through the apparatus by means of a pump, which is connected to stage two of the TSI. Air is sucked through the apparatus from the mouth, flows through

upper tubing via the upper impinger and the lower tubing to
the lower impinger where it bubbles through liquid and exits
the apparatus via outlet pipe. The liquid in the upper
impinger traps any particle with a size such that it is
unable to reach stage two of the TSI. Fine particles, which
are the particles able to penetrate to the lungs in the
respiratory tract, are able to pass into stage two of the TSI
where they flow into the lower impinger liquid.

30ml of distilled water is put into the lower impinger

10 and 7 ml of distilled water is put into the upper impinger.

The pump is adjusted to give an air flow rate of 60 litres

per minute in the apparatus.

The inhaler device is weighed. The mouthpiece of the inhaler device is connected to the mouth of the TSI, the inhaler is actuated to dispense a dose of the powder and the pump is switched on and timed for a period of ten seconds. The pump is then switched off and the inhaler is removed from the TSI, re-weighed and the amount of powder lost from the inhaler calculated.

The sections of the apparatus making up stage one of the TSI are washed into a second flask and made up to 250 ml with distilled water. The sections making up the second stage of the TSI are washed into a third flask and made up to 100 ml with distilled water.

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The amount of active substance in each section of the TSI is measured for each test. The following method may be used.

The contents of the flasks containing the washings from the stages of the TSI are assayed using High Performance Liquid Chromatography (HPLC) analysis for the content of the active material and compared against standard solutions containing, for example, 0.5 μ g ml⁻¹ and 1 μ g ml⁻¹ of the active material.

The percentage of the active material in each stage of the TSI is calculated from the standard response for each test and the mean for the tests may be calculated to give an indication of the proportion of the active particles reaching the second stage of the TSI apparatus. The respirable

15 fraction (fine particle fraction) is calculated as the percentage of the total amount of drug emitted from the inhaler device that reaches stage two of the TSI and gives an indication of the proportion of active particles which would reach the deep lung in a patient.

20

Multi-Stage Liquid Impinger

Powder blends were also tested in a Multi-Stage Liquid

Impinger (MSLI) (European Pharmacopoeia 2.9.18.) as indicated

25 above to assess the efficiency of the delivery of the active

particles to the lungs of a patient by an inhaler device.

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The MSLI is a five-stage separation device used in the assessment of the fine particle characteristics of particle clouds generated using oral inhalation devices.

Impaction stage 1 is the pre-separator and stage 5 is an integral filter stage. An impaction stage comprises an upper horizontal metal partition wall through which a metal inlet jet tube with its impaction plate is protruding.

In use, a suitable low resistance filter capable of quantitatively collecting the active material is placed in stage 5. The apparatus is assembled and connected to a flow system. For the examples below, a flow rate of 90 litres per minute was used.

20 ml of a solvent is dispensed into each of stages 1 to
4. With the pump running, the mouthpiece of the inhaler
15 device is located in the mouthpiece adapter of the MSLI and
the inhaler device is discharged.

The amount of active ingredient in each stage of the apparatus is determined, for example using the method described in European Pharmacopoeia 2.9.18. Thus the fine particle dose can be calculated.

For the following examples, the inhaler device used in the TSI and MSLI tests was the Monohaler (manufactured by Miat, Italy).

Example 3

Powder blends were produced for testing in the TSI apparatus.

The blends were produced by a standard sequence of the following steps

- 5 i. Mixing in a Turbula mixer (a tumbling blender) for between 30 minutes and 1 hour at fast speed;
 - ii. Passing the blend through a series of 600μm, 420μm and 355μm aperture diameter sieves to improve mixing and to help break up stable agglomerates;
- 10 iii. Mixing the blend further in the Turbula mixer for between 30 minutes and 1 hour at a slow speed; and
 - iv. Filling the blend into gelatine capsules for use in the Monohaler, each capsule containing about 5 mg of the blend.
- Various powder blends were prepared comprising an active material, salbutamol sulphate, and an additive material.

 Several of the blends included low-density leucine in accordance with the invention as the additive material. The low-density leucine was prepared by an aerosol method as
- 20 described in Example 2 above. Other blends included no additive material or Aerosil (trade name of Degussa for colloidal silicon dioxide) or conventional milled leucine as the additive material to give comparative results. The percentages given for the amount of additive material in the
- 25 blend is the percentage by weight of the additive based on the weight of the active material and additive material.

The % given for the amount of components in the blends is the % by weight of the component based on the weight of the powder blend.

Table 4

Sample	Mean mass of active material left in capsule(mg)	Mean respirable fraction (%)	
Salbutamol	3.7	27	
Salbutamol + 2% Aerosil	1.7	75	
Salbutamol + 1% milled leucine	2.3	14	
Salbutamol + 10% milled leucine	2.3	13	
Salbutamol + 1% low-density leucine	3.4	51	
Salbutamol + 10% low-density leucine	2.3	31	
Salbutamol + 20% low-density leucine	1.3	15	

5

The table shows that the addition of the low-density leucine improved the respirable fraction of the active material.

Particularly good results were obtained where the percentage by weight of the low-density leucine was 1%.

10

Micronised salbutamol powder itself is difficult to handle, being cohesive and adhesive and significantly affected by static. The powder forms hard compact agglomerates and sticks to or jumps from surfaces due to electrostatic forces. The addition of 1% and 10% by weight

of milled leucine improved the powder flow and handling performance of the salbutamol powder. The mixes including 1% and 10% by weight of the low-density leucine had significantly improved powder flow characteristics, with minimal adhesion to glass walls compared with the milled leucine mixes.

Example 4

- The effect of the proportion of low-density leucine in the powder blend was determined by testing blends containing salbutamol sulphate and various percent by weight of low-density leucine. The effect of the method of blending was also investigated by combining the following mixing methods:
- 15 HS high shear mixing using a food processor having a metal blade
 - LS low shear mixing using a pestle and mortar and sieving
 S sieving
 - T mixing in a tumbling blender (Turbula mixer)
- 20 The blends were tested using the TSI. The dose in each capsule of the powder blend was about 5 mg. Each test was repeated with a total of two capsules (a total of 10 mg of powder blend). The results are shown in Table 5.

The % given for the amount of components in the blends
25 is the % by weight of the component based on the weight of
the powder blend.

Table 5

% by weight of low-density leucine	Mixing protocol	Mean mass of drug left in capsule (mg)	Mean respirable fraction (%)	
None		3.7	27	
1.0	нѕ	4.7	56	
1.0	HS, S, T	3.6	60	
1.0	LS, S, T	4.0	69	
2.5	LS, S, T	3.7	64	
5.0	LS	4.4	59	
5.0	LS, S, T	3.6	66	
7.5	LS	3.6	60	
7.5	LS, S, T	3.2	73	

- Thus it can be seen that the addition of low-density leucine gave a significant increase in the respirable fraction of the active material although, in each case, a large proportion of the active material remains in the device on actuation of the inhaler.
- Salbutamol sulphate micronised powder is less difficult to handle than the salbutamol base powder but does exhibit cohesive and adhesive nature. While the addition of leucine gave some improvement in the powder flow and handling performance, the addition of the low-density leucine gave

significantly improved powder flow and handling characteristics.

Example 5

5 Powder blends for inhalation comprising active material, low-density leucine and lactose diluent were tested using a multi-stage liquid impinger (MSLI) using a flow rate of 90 litres per minute. The blends were prepared by mixing the active material and low-density leucine using the method described in respect of Example 3 above. The active material used was salbutamol sulphate and the low-density leucine was prepared by aerosolisation as described in Example 2 above. The mixture was then mixed with lactose. Two grades of lactose were used. Sorbolac (400) comprises lactose fines having an effective particle diameter of 7μm and Lactochem comprises lactose having a particle size between 63μm and 90μm obtained by sieving. Capsules for testing were filled with between 20mg and 25mg of the powder blend.

The results of the MSLI tests are shown in Table 6. The 20 % shown are the % by weight of the material based on the weight of the powder blend.

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Table 6

% of low- density leucine	% of lactose and grade	Active material left in the device (%)	Respirable fraction (%)
1.0	50 Sorbolac	21	65
7.5	90 Lactochem	11	55
7.5	90 Sorbolac	14	59

Thus it can be seen that the high respirable fraction is maintained on the inclusion of the lactose but the emptying of the capsule in improved compared with the blends which do not contain the lactose.

The use of the low-density leucine material has been described above in relation to its use in powders for pharmaceutical use, in particular in powders for inhalation for which the powder properties are of great importance.

The low-density amino acid of the present invention may

also be used in other pharmaceutical applications. The lowdensity leucine may be used, for example, in powder

formulations for tabletting. The advantageous properties, in

particular the flow properties, would improve the performance
of the powder in the pressing of tablets.

The low-density amino acid may also be used as an additive in powders to be filled into capsules. The improved flow and handling characteristics of the powders containing the low-density amino acid would give improved filling and emptying of the capsules.

There are several additive materials currently available and which are routinely added to powders to improve their flow properties, for example Aerosil (colloidal silica). A significant advantage of amino acids compared with, for example, silica is that amino acids are more pharmaceutically acceptable, in particular for inhalation into the lung.

A further advantage of some amino acids, in particular leucine, over silica is that, unlike silica, leucine dissolves in water to give a clear solution. It is envisaged, therefore, that the low-density amino acid, for example leucine, could advantageously be used in powders for use as diagnostic reagents for which the ability to form a clear solution may be essential.

It also envisaged that the low-density amino acids may
find application in fields other than pharmaceutical field.
For example, the low-density amino acid may be used in dry
powders for fire suppressants, for example to improve the
powder properties of powders in dry powder fire
extinguishers.

Claims:

- 1. Amino acid particles in which a sample of the particles has a bulk density not more than 0.1 gcm⁻³.
- 5 2. Amino acid particles according to claim 1, in which a sample of the particles has a bulk density not more than 0.05 gcm⁻³.
 - 3. Amino acid particles having a mass median aerodynamic diameter (MMAD) not more than $10\mu m$.
- 10 4. Amino acid particles according to claim 3, in which the particles have a MMAD not more than $5\mu m$.
 - 5. Amino acid particles being in the form of flakes having a thickness of not more than $0.5\mu m$.
- 6. Amino acid particles according to claim 5 in which the 15 flakes have a thickness of not more than 100nm.
 - 7. Amino acid particles according to any preceding claim, in which the amino acid is leucine.
- A powder for use in a dry powder inhaler, the powder including active material and amino acid particles according
 to any of claims 1 to 7.
 - 9. A powder according to claim 8, in which the powder includes not more than 20% by weight of amino acid based on the weight of the powder.

- 10. A power according to claim 9, in which the powder includes not more than 10% by weight of amino acid based on the weight of the powder.
- 11. A powder according to claim 8 or claim 9, the powder 5 further including particles of a diluent.
 - 12. A powder according to claim 11, in which the diluent has a particle size such that at least 90% by weight of the diluent particles have a particle size not more than $10\mu m$.
 - 13. A powder according to claim 11, in which the diluent
- 10 has a particle size such that at least 90% by weight of the diluent particles have a particles size not less than 50µm.
 - 14. A powder according to claim 11, in which the diluent has a fine particle portion having a particle size such that at least 90% by weight of the particle of the fine particle
- particle portion having a particle size such that at least 90% by weight of the particles of the coarse particle portion have a particle size not less than 50μm.
- 15. A powder according to claim 14, in which the fine
 20 particle portion and coarse particle portion comprise the
 same material.
 - 16. A powder according to any of claims 11 to 15, in which the diluent includes a crystalline sugar.

- 17. A powder according to any of claims 14 to 16, in which the powder includes not more than 5% by weight of the fine particle portion based on the weight of the powder.
- 18. A powder according to any of claims 14 to 17, in which
 5 the powder includes not more than 95% by weight of the coarse
 particle portion based on the weight of the powder.
 - 19. A dry powder inhaler, the inhaler containing powder according to any of claims 8 to 18.
- 20. A method of preparing particles of amino acid the

 10 method including the step of forming solid amino acid

 particles from a vapour or in a solvent, the method being

 such that the particles are formed while being suspended in a

 gas flow.
- 21. A method of preparing particles of amino acid, the
 15 method including the step of condensing amino acid vapour to
 form solid amino acid particles.
 - 22. A method according to claim 20 or claim 21, in which particles of amino acid are formed by aerosol condensation.
- 23. A method according to claim 21 or claim 22, in which the 20 method includes the steps of
 - a) heating the amino acid so that the amino acid forms a vapour;
 - b) mixing the amino acid vapour with cool air to form a cloud of condensed amino acid particles; and
- c) collecting the condensed particles.

- 24. A method according to any of claims 21 to 23, the method including the step of heating the amino acid particles to a temperature of at least 150°C at ambient pressure.
- 25. A method of producing particles of amino acid, in which 5 droplets of amino acid in a solvent are dried to form solid particles of amino acid.
 - 26. A method according to claim 20 or claim 25, in which the method includes the step of spray drying to form solid particles of amino acid.
- 10 27. A method according to claim 25 or claim 26, in which the material to be dried comprises amino acid in solution.
 - 28. A method according to claim 27, in which material to be dried comprises amino acid in aqueous solution.
 - 29. A method according to any of claims 25 to 28 in which
- 15 the droplets dried have a mean size of not more than $10\,\mu m$.
 - 30. A method according to any of claims 20 to 29, in which the method is such that the MMAD of the solid amino acid particles produced is not more than $10\mu m$.
 - 31. A method of producing amino acid particles, the method
- 20 being such that the amino acid particles produced are amino acid particles according to any of claims 1 to 7.
 - 32. A method of producing particles of amino acid according to any of claims 1 to 7.
- 33. Particles of amino acid obtainable by a method according 25 to any of claims 20 to 31.

- 34. A method of making a powder according to any of claims 8 to 18, the method including the steps of mixing amino acid according to any of claims 1 to 7 or claim 33 with active material.
- 5 35. A method of making a powder according to any of claims
 11 to 18, the method including the step of mixing amino acid
 according to any of claims 1 to 7 or claim 33 with active
 material followed by the step of mixing the leucine and
 active material with a diluent.
- 10 36. Use of particles of amino acid according to any of claims 1 to 7 or claim 33 in a powder to improve the flow properties of the powder.
- 37. Use of particles of amino acid according to any of claims 1 to 7 or claim 33 in a powder for use in a dry powder 15 inhaler.
 - 38. Particles of amino acid being substantially as herein described.
 - 39. A method of producing particles of amino acid, the method being substantially as herein described.
- 20 40. A powder for inhalation, the powder being substantially as herein described.

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(57) Abstract

Particles of an amino acid such as leucine may be formed from an amino acid vapour, for example by aerosol condensation, or by spray drying. The amino acid particles have a bulk density of not more than 0.1 gcm⁻³ or have a mass median aerodynamic diameter of not more than 10 μ m or are in the form of flakes having a thickness of not more than 100 μ m. The inclusion of the particles of amino acid in powder for use in dry powder inhalers has been found to improve the respirable fraction of the active material in the powder.

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leucine having a low-density shows flow enhancing properties when added to powders. In particular, the addition of the low-density leucine to a powder gives improved glidant properties as well as improved anti-adherent properties.

Where reference is made to "density" in this specification, it is to be understood as being a reference to bulk density unless it is clear from the context that a different measurement of density is being referred to.

5

Advantageously, the amino acid particles have a bulk

10 density not more than 0.1 gcm⁻³ and preferably not more than

0.05 gcm⁻³.

The invention also provides amino acid powder, the powder having a bulk density of not more than 0.1 gcm⁻³.

A second aspect of the invention provides amino acid

15 particles having a mass median aerodynamic diameter (MMAD) of

not more than 10µm. Preferably, the MMAD is not more than

5µm. Reference is made above to the MMAD of the particles.

Where the particles have a low bulk density in accordance

with the first aspect of the invention, the actual diameter

20 of the particles can be relatively large while the MMAD is

still small enough for the desired aerodynamic

characteristics of the particles.

Alternatively, the size distribution of the particles can be characterised by their volume mean diameter (VMD).

25 Advantageously, the VMD of the amino acid particles is not more than $10\mu m$, preferably not more than $5\mu m$.

In some cases, the particles of the third aspect of the invention will also have the desired MMAD (or VMD) of the second aspect of the invention.

It has been found that the thin flakes of leucine in accordance with this further aspect of the invention generally have a low density and improved flow properties.

It has been found to be particularly advantageous for the leucine to be in the form of flakes having a thickness of less than about 100nm.

It has been found that when, for example, the leucine flakes have been prepared using the spray drying method described below, that they have a very small thickness of less than 100nm and a relatively large width. It has been found that the flakes may become fractured during subsequent processing of the powder but that the beneficial properties of the flakes are not substantially diminished. It is thought, therefore, that it is the very small thickness of the flakes which gives their advantageous properties.

The aspect ratio of the flakes of amino acid can be

considered to be the (width of the particles)/(thickness of
the particles). Advantageously the aspect ratio of the
particles is at least 200, preferably at least 500.

Observation of the thickness of the flakes may be made by studying electron microscope (SEM) images of the 25 particles. For example, flakes may be mounted on an electron and the temperature required to form a vapour of that amino acid.

According to a further aspect of the invention, in the method of producing particles of amino acid, droplets of amino acid in a solvent are dried to form solid particles of amino acid.

Advantageously, the method includes the step of spray drying amino acid in a solvent.

Advantageously, the material to be dried comprises amino 10 acid in solution, which is advantageously an aqueous solution.

Where the amino acid is one which sublimes, for example leucine, it is thought that it may be advantageous for some sublimation of the leucine to take place during the spray drying of the leucine to give the most advantageous morphology of the leucine particles produced. In such a case, advantageously, the spray drying method is such that at least some of the amino acid sublimes during the spray drying.

20 Conventional spray drying of the amino acid may produce large particles of amino acid which are generally spherical in shape. Where the amino acid is leucine, such particles may have a particle diameter of 40μm or more. Such leucine particles produced by a spray drying method are described in 25 Pharmaceutica Acta Helvetiae 70(1995) 133-139. Such

Claims:

- 1. Amino acid particles in which a sample of the particles has a bulk density not more than 0.1 gcm⁻³.
- 5 2. Amino acid particles according to claim 1, in which a sample of the particles has a bulk density not more than $0.05~{
 m gcm}^{-3}$.
 - 3. Amino acid particles having a mass median aerodynamic diameter (MMAD) not more than $10\mu m$.
- 10 4. Amino acid particles according to claim 3, in which the particles have a MMAD not more than 5μm.
 - 5. Amino acid particles being in the form of flakes having a thickness of not more than $0.5\mu m$.
- 6. Amino acid particles according to claim 5 in which the 15 flakes have a thickness of not more than 100nm.
 - 7. Amino acid particles according to any preceding claim, in which the amino acid is leucine.
- A powder for use in a dry powder inhaler, the powder including active material and amino acid particles according
 to any of claims 1 to 7.
 - 2. A powder according to claim 8, in which the powder includes not more than 20% by weight of amino acid based on the weight of the powder.

- 10. A power according to claim 9, in which the powder includes not more than 10% by weight of amino acid based on the weight of the powder.
- 11. A powder according to claim 8 or claim 9, the powder 5 further including particles of a diluent.
 - 12. A powder according to claim 11, in which the diluent has a particle size such that at least 90% by weight of the diluent particles have a particle size not more than $10\mu m$.
 - 13. A powder according to claim 11, in which the diluent
- 10 has a particle size such that at least 90% by weight of the diluent particles have a particles size not less than 50μm.
 - 14. A powder according to claim 11, in which the diluent has a fine particle portion having a particle size such that at least 90% by weight of the particle of the fine particle
- particle portion having a particle size such that at least 90% by weight of the particles of the coarse particle portion have a particle size not less than 50μm.
- 15. A powder according to claim 14, in which the fine20 particle portion and coarse particle portion comprise the same material.
 - 16. A powder according to any of claims 11 to 15, in which the diluent includes a crystalline sugar.

- 17. A powder according to any of claims 14 to 16, in which the powder includes not more than 5% by weight of the fine particle portion based on the weight of the powder.
- 18. A powder according to any of claims 14 to 17, in which
 5 the powder includes not more than 95% by weight of the coarse particle portion based on the weight of the powder.
 - 19. A dry powder inhaler, the inhaler containing powder according to any of claims 8 to 18.
- 20. A method of preparing particles of amino acid the

 10 method including the step of forming solid amino acid

 particles from a vapour or in a solvent, the method being

 such that the particles are formed while being suspended in a

 gas flow.
- 21. A method of preparing particles of amino acid, the
 15 method including the step of condensing amino acid vapour to form solid amino acid particles.
 - 22. A method according to claim 20 or claim 21, in which particles of amino acid are formed by aerosol condensation.
- 23. A method according to claim 21 or claim 22, in which the 20 method includes the steps of
 - a) heating the amino acid so that the amino acid forms a vapour;
 - b) mixing the amino acid vapour with cool air to form a cloud of condensed amino acid particles; and
- 25 c) collecting the condensed particles.

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- 24. A method according to any of claims 21 to 23, the method including the step of heating the amino acid particles to a temperature of at least 150°C at ambient pressure.
- 25. A method of producing particles of amino acid, in which 5 droplets of amino acid in a solvent are dried to form solid particles of amino acid.
 - 26. A method according to claim 20 or claim 25, in which the method includes the step of spray drying to form solid particles of amino acid.
- 10 27. A method according to claim 25 or claim 26, in which the material to be dried comprises amino acid in solution.
 - 28. A method according to claim 27, in which material to be dried comprises amino acid in aqueous solution.
 - 29. A method according to any of claims 25 to 28 in which
- 15 the droplets dried have a mean size of not more than 10μm.
 - 30. A method according to any of claims 20 to 29, in which the method is such that the MMAD of the solid amino acid particles produced is not more than $10\mu m$.
 - 31. A method of producing amino acid particles, the method
- 20 being such that the amino acid particles produced are amino acid particles according to any of claims 1 to 7.
 - 32. A method of producing particles of amino acid according to any of claims 1 to 7.
- 33. Particles of amino acid obtainable by a method according 25 to any of claims 20 to 31.

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34. A method of making a powder according to any of claims 8 to 18, the method including the steps of mixing amino acid according to any of claims 1 to 7 or claim 33 with active material.

- 5 35. A method of making a powder according to any of claims
 11 to 18, the method including the step of mixing amino acid
 according to any of claims 1 to 7 or claim 33 with active
 material followed by the step of mixing the leucine and
 active material with a diluent.
- 10 36. Use of particles of amino acid according to any of claims 1 to 7 or claim 33 in a powder to improve the flow properties of the powder.
- 37. Use of particles of amino acid according to any of claims 1 to 7 or claim 33 in a powder for use in a dry powder 15 inhaler.
 - 38. Particles of amino acid being substantially as herein described.
 - 39. A method of producing particles of amino acid, the method being substantially as herein described.
- 20 40. A powder for inhalation, the powder being substantially as herein described.

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INTERNATIONAL APPLICATION PUBLISHED UNDER THE PATENT COOPERATION TREAT

INTERNATIONAL APPLICATION POBLIST	TLD (ONDER THE PATENT COOPERATION TREATT (PCT)
(51) International Patent Classification 7:		(11) International Publication Number: WO 00/33811
A61K 9/00	A2	(43) International Publication Date: 15 June 2000 (15.06.00)
(21) International Application Number: PCT/GB (22) International Filing Date: 9 December 1999 ((30) Priority Data: 9827145.5 9 December 1998 (09.12.98)	09.12.9	BR, BY, CA, CH, CN, CR, CU, CZ, DE, DK, DM, EE,
(71) Applicant (for all designated States except US): VI LIMITED [GB/GB]; 12 St. James's Square, Londo 4RB (GB).		A BE, CH, CY, DE, DK, ES, FI, FR, GB, GR, IE, IT, LU,
(72) Inventors; and (75) Inventors/Applicants (for US only): GANDERTO [GB/GB]; Crooked Chimneys, Cheriton Bishop, Ex- 6JL (GB). MORTON, David, Alexander, Vodden 2nd Floor Flat, Linsley House, Beechen Cliff Re BA2 4QR (GB). LUCAS, Paul [GB/GB]; 5 F Close, Felderland Lane, Worth, Deal CT14 0PB (6)	keter EX [GB/GI oad, Ba celderla	(6 Without international search report and to be republished upon receipt of that report. th
(74) Agents: HUMPHREYS, Ceris, Anne et al.; Abel & Red Lion Street, London WC1R 4PQ (GB).	Imray,	20
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(54) Title: IMPROVEMENTS IN OR RELATING TO P	OWDE	RS
(57) Abstract		·
spray drying. The amino acid particles have a bulk densi	ty of no	from an amino acid vapour, for example by aerosol condensation, or by the more than 0.1 gcm ⁻³ or have a mass median aerodynamic diameter of the contract of the more than 100 μ m. The inclusion of the particles of amino improve the respirable fraction of the active material in the powder.
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INTERNATIONAL PRELIMINARY EXAMINATION REPORT

(PCT Article 36 and Rule 70)

Applicant's	or age	ent's file reference	T		O Natific		· · · · · · · · · · · · · · · · · · ·
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ational Application No

PCT/GB 99/04156

A. CLASSIFICATION OF SUBJECT MATTER
IPC 7 A61K9/00 A61K9/14

A61K9/72

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols) IPC 7-A61K

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practical, search terms used)

WPI Data, PAJ, CHEM ABS Data

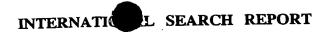
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Date of mailing of the international search report 04/07/2000
Authorized officer Scarponi, U



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Int ional Application No PU 96/01783

A. CLASS	IFICATION OF SUBJECT MATTER		
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Date of the	actual completion of the international search	Date of mailing of the international se	arch report
2	9 October 1996	1 2. 11. 9	6
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